

EMISSION AND FUEL CONSUMPTION STUDIES USING SEPARATED AT LOW TEMPERATURES PURE RAPESEED OIL

Vladimir Baks, Ilmars Dukulis, Aivars Birkavs

Latvia University of Agriculture

bladimirs_baks@inbox.lv, ilmars.dukulis@llu.lv, aivars.birkavs@llu.lv

Abstract. Pure rapeseed oil is an environmentally friendly alternative fuel. Its production and storing processes are not toxic for flora and fauna. One of the problems to use rapeseed oil as a biofuel is its higher melting point in comparison with fossil diesel fuel. If the length of the fatty acids chains is the same, increasing of double bonds quantity lowers the melting and solidification temperature that allows the use of vegetable oil containing unsaturated fatty acids as fuel without warming up at lower ambient temperatures. However, when vegetable oils are highly unsaturated, they solidify at lower temperatures, but have high oxidative instability – they quickly break down. Another problem is fuel consumption – rapeseed oil is less economical than diesel fuel and some emission parameters running the engine on rapeseed oil are worse than using diesel. The difference of the melting temperature allows separating such components as sulphur and phosphorus as integral components of molecules. Sulphur in rapeseed oil is in the form of organic compounds, which are decomposition products of glucosinolates. Fractionation can help remove waxes and other nontriglycerides, naturally occurring high-melting point triglycerides formed during hydrogenation – in such a way it is possible to get rapeseed oil with different properties than for conventional one. The research results show that for oil improvement material and time resources are consumed, but no significant benefits for fuel economy and exhaust gas composition were observed, that is why such an oil enriching method is applicable only during the winter months, because it allows using the oil as a fuel at lower temperatures.

Keywords: rapeseed oil, fractionation, exhaust gases.

Introduction

Vegetable oils by 95 to 97 % consist of fatty acid triglycerides. The residues of fatty acids are responsible for the chemical and physical properties of oils. If the length of the fatty acid chains is the same, increasing of double bond quantity lowers the melting and solidification temperature that allows the use of vegetable oil containing unsaturated fatty acids as a fuel without warming up at lower ambient temperatures. Such a fact is very important for using rapeseed oil as an environment friendly fuel in winter months. February of 2011 with average monthly air temperature -8.9°C (4.1 degrees below the normal) was the 13th Latvian coldest one in the last 88 years. In such a way the rapeseed oil as a fuel cannot be used. That is why it is necessary to modify such kind of fuel for using it in winter months, too [1].

It is possible to divide rapeseed oil into fractions after solidification. Fractionation (winterizing as it is sometimes called) helps remove the high-melting point triacylglycerols (TAGs) – in such a way we can get the liquid phase which is more resistant to lower temperatures. The process involves chilling the fat and then separating the two phases by filtration. One of the key factors determining the success of the fractionation process is the efficiency of separation. During this cycle, agitation is introduced by either very slow rotation of mechanical agitators or by bubbling cold air through the cell. After a certain period, the temperature difference is changed for the crystal maturing phase, and the agitation may be reduced or stopped. Although the TAGs form the main crystalline phase, the minor components, or impurities, can often play a large role in how crystallization occurs and crystallization may be substantially different in refined oil than in the unrefined starting material.

Lutton stated that if the fatty acids of a TAG differ in length by more than four carbons, it forms a triple chain-length structure. Triple chain-length packing is also observed in TAG containing a cis-unsaturated fatty acid because this causes a kink in the structure. Cis-unsaturated fatty acids do not mix in one layer with saturated fatty acids, and triple chain-length crystals are formed. It should be noted that trans-unsaturated fatty acids incorporate into a crystal structure in the same way as the saturated fatty acids [2].

Transformation of unstable to stable polymorphs can be achieved by a slight increase in temperature above the melting point of the less stable forms. This increase in temperature first causes the melting of the unstable forms and then solidification in a more stable form [2; 3].

Saturated fatty acids have a straight hydrocarbon chain. A trans-double bond is accommodated with a little change in the shape, but natural fatty acid residues of pure plant oils are usually located in cis-configuration of the molecular form. Cis-configuration is the dimensional position, when the radicals are located on one side of the double bond. This situation causes 'the windings' in the molecular geometry – therefore the chains cannot go closer and establish hydrophobic intermolecular contacts. Rapeseed oil contains a large amount of cis-configured unsaturated fatty acids as linolenic acid; therefore it has higher fluidity [2; 3].

Trans-acids have melting points much closer to those of the corresponding saturates. Polymorphism results in two or more solid phases with different melting points. Methyl esters are lower melting than fatty acids but follow similar trends [2; 4; 5].

Getting more unsaturated form of rapeseed oil is important because this form has lower viscosity, and deep freezing is harmful for rapeseed oil as a biofuel. The kinematical viscosity can be increased with elongation of chains, hydrogenation, polymerisation or oxidation. The first two reactions need specific conditions, but heating stimulates the polymerisation or oxidation process. So, it can be suggested that deep freezing stimulates conversion of cis-unsaturated forms into trans-unsaturated TAGs forms as these structures have viscosity comparable with fully saturated. The previously made experiments showed, that the kinematical viscosity of the fluid was changed from $59.56 \text{ mm}^2 \cdot \text{s}^{-1}$ (pure rapeseed oil) to $58.78 \text{ mm}^2 \cdot \text{s}^{-1}$ (rapeseed oil after freezing and phase separation) [6].

The LEAR type rape (low erucic acid rapeseed) is the most popular in Latvia. The high tolerance of erucic acid to temperature makes it suitable for transmission oil. Its ability to polymerize and dry means: it can be and is used as a binder for oil paints. Being a hydrocarbon of a high calorific value, with a very low flash point, high cetane number, and good lubrication qualities, erucic acid can be a valuable component of biodiesel. But as high erucic varieties of rape are rich in this C22 monoene acid, the viscosity of HEAR (high erucic acid rapeseed) oil is significantly higher than that of canola oil – from this point of view LEAR can be more perspective for usage as a biofuel [5; 7].

Alternative fuel sphere researches in the whole world are directed on decreasing the dependence on oil extraction industry, updating the world economics and defending environment from pollution. Environmental pressures demand cleaner processes, and there is a market for new 'green' chemistry products. The usage of pure plant oils is a way to live in close connection with nature. Generally, renewable fuels are produced to reduce greenhouse gas emissions, improve combustion of fuels, and extend supplies of fossil fuels, although their production may also be used to subsidize the production of agricultural commodities and improve the balance of trade for countries that produce little fossil fuel.

The subject of the research is emission and fuel consumption studies using separated at low temperatures pure rapeseed oil in comparison with conventional rapeseed oil and fossil diesel fuel.

Materials and methods

During the experiment the LEAR type rapeseed oil from rape grown in Latvia was used. It can be used for both purposes: as a food product and biofuel.

To get rapeseed oil with lower viscosity than pure rapeseed oil has, using the experience from the previously made experiments [6], 15 l of pure rapeseed oil were taken. This oil was frozen in a freezer at $-12 \text{ }^\circ\text{C}$. After 36 hours, when the crystallization process of oil takes a visual maximum (the oil was constant in 5 hours), the solid phase was separated. From 15 l of pure rapeseed oil 9 l of oil with lower viscosity (further – enriched) were obtained. The output of the product was 60 %.

The enriched oil was compared with diesel fuel and conventional pure rapeseed oil. The points of comparing were the fuel consumption and components of exhaust gases.

During the experiment the Opel 16 DA diesel engine was used. The Opel 16 DA diesel engine is a single line 4/OHC engine, having a capacity of 1598 cm^3 , the compression ratio – 23 and the power of 40 kW. The engine fuel system was powered by a fuel pump Bosch VE 4/9R215. The research was done on the test bench. The engine was equipped with Elsbett two-tank system (Fig. 1), but the engine revolution frequency was measured by the stroboscope DG 85.

The fuel consumption was determined using the *KERN 440-49A* electronic weighing system which provides measurements with an accuracy of 0.1 g at intervals of 1 second. The weighing system management and data registration is computer controlled.

The exhaust gases were measured using the *AVL SESAM (System for Emission Sampling and Measurement)* multicomponent exhaust gas measurement system. This system is based on the *FTIR (Fourier Transform Infrared Spectroscopy)* optical measurement method that gives an opportunity to detect a large amount of exhaust gases components at intervals of 1 second.

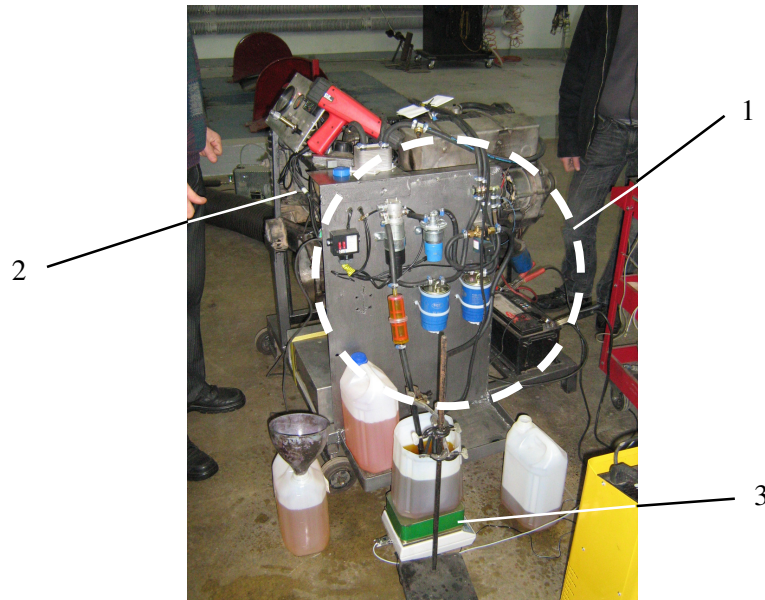


Fig. 1. Engine test bench:

1 – *Elsbett* two-tank system; 2 – diesel engine; 3 – weighing system

During the experiment the engine revolution frequencies 900 rpm, 1600 rpm and 2500 rpm were used.

The results of the measurements were automatically saved in a digital format and imported in a spreadsheet program for analyzing.

Results and discussion

The data in Table 1 show that the fuel consumption of the enriched rapeseed oil (compared with pure rapeseed oil) was less at all test modes.

Table 1

Fuel consumption measurement results

Fuel	900 rpm	1600 rpm	2500 rpm
Diesel, g·h ⁻¹	396.8	1028.1	1558.6
Rapeseed oil, g·h ⁻¹	559.0	1115.1	1735.5
Enriched rapeseed oil, g·h ⁻¹	558.7	1071.4	1723.7

The largest fuel consumption difference was observed at 1600 rpm, when between the enriched and pure rapeseed oil it was 4 %. It was higher than the diesel fuel consumption only by 4 %. At 900 rpm and 2500 rpm the difference between the enriched and conventional rapeseed oil was not significant.

As the working hypothesis suggested, the enriched rapeseed oil would not be worse than conventional rapeseed oil also comparing the exhaust emissions, therefore all three fuel types were tested at the same engine working modes.

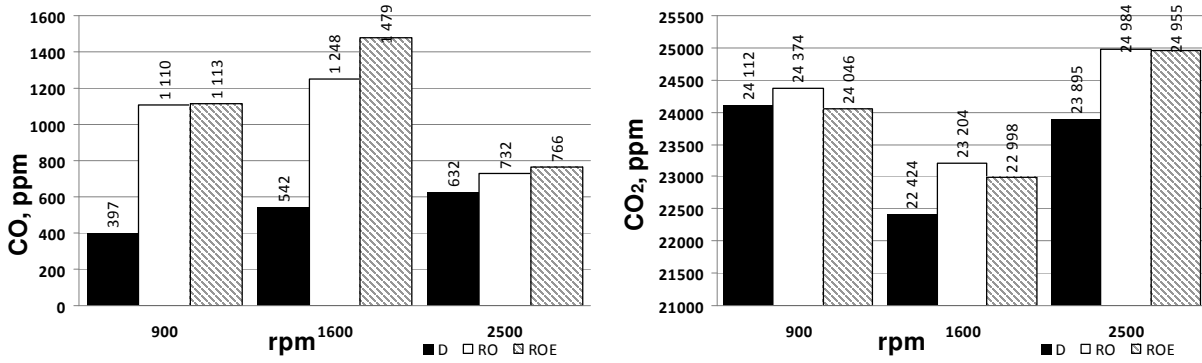


Fig. 2. CO and CO₂ measurement results: D – diesel fuel, RO – rapeseed oil, ROE – enriched oil

Comparing the amount of CO₂ and CO in exhaust gases (Fig. 2), that affect each other, CO quantity using the enriched rapeseed oil was a little bit higher (what is correlating with a little bit less CO₂) as for the conventional rapeseed oil. But in absolute numbers the amount of CO₂ and CO was very close. Of course, both values are higher in comparison with diesel fuel.

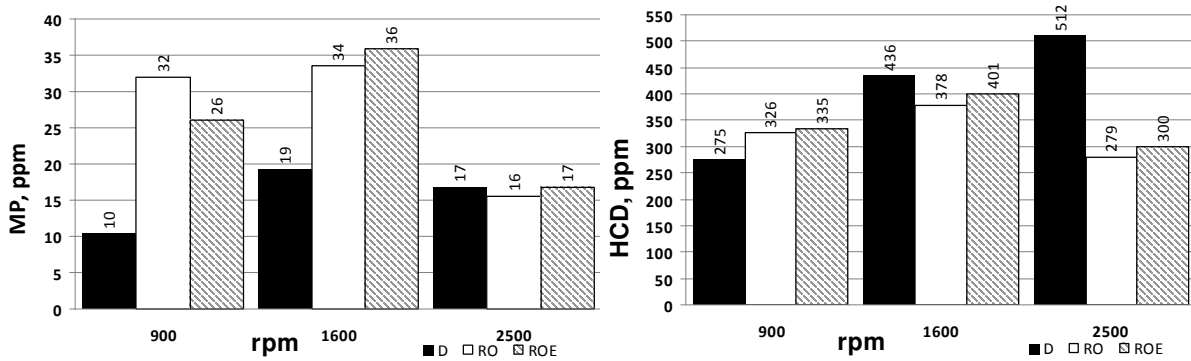


Fig. 3. MP and HCD measurement results: D – diesel fuel, RO – pure oil, ROE – enriched oil

The data in Figure 3 show that the quantity of MP (mechanical particles) at 900 rpm and 1600 rpm using diesel fuel was less than for both oils. At 2500 rpm the content of MP in emissions decreased about twice and it was practically equal (even a little less) with diesel fuel. The quantity of HCD (unburned hydrocarbons) at 900 rpm using diesel fuel was less than for both oils, but at 1600 and 2500 rpm the content of HCD using the enriched rapeseed oil was correspondingly less by 8 % and 41 % than for diesel.

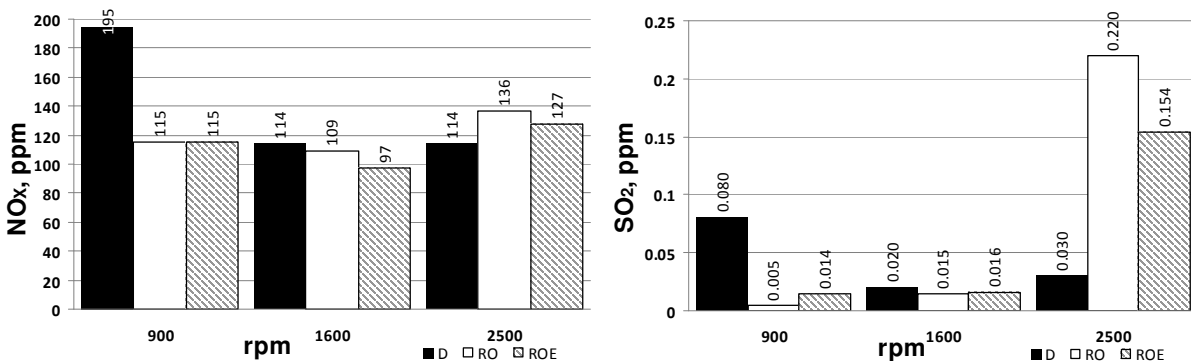


Fig. 4. NO_x and SO₂ measurement results: D – diesel fuel, RO – rapeseed oil, ROE – enriched oil

As it can be seen from Figure 4, at 900 and 1600 rpm for both oils the content of NO_x was less than for diesel, but at 2500 rpm small increasing of NO_x was observed – the difference between diesel fuel and pure rapeseed oil was 16 %, but between diesel fuel and the enriched oil – 11 %.

At 900 and 1600 rpm the content of SO₂ using both oils was less than for fossil diesel. The 2500 rpm mode showed a very sharp increase also for this component – by 86 % for rapeseed oil and 80 % for the enriched oil. The SO₂ content difference between the enriched oil and unimproved oil was 30 %.

The CO, CO₂, SO₂ and MP content analysis at 2500 rpm shows, that in conditions of temperature increasing (1) the available CO quantity for SO₂ electrons accepting in a reduction-oxidation reaction (2) was decreasing; therefore the SO₂ content is growing, and the amount of MP (and pure sulphur as a part of this measurement) is decreasing.



Conclusions

1. When operating the engine on the enriched rapeseed oil the fuel consumption in average was about 2 % lower compared to the conventional rapeseed oil. The largest difference, i.e., 4 % was observed at the 1600 rpm, but for both oils the consumption is still much higher than for fossil diesel fuel.
2. The impact of using the enriched rapeseed oil on environment is almost the same as using the conventional rapeseed oil, because decreasing in average the amount of CO₂, mechanical particles and NO_x, other components – CO, unburned hydrocarbons and SO₂ – slightly increase.
3. Considering that for the oil improvement material and time resources are consumed, but no significant benefits for fuel economy and exhaust gas composition were observed, such an oil enriching method is applicable only during the winter months, because it allows to use the oil as a fuel at lower temperatures.

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